Greenhouse gas emissions from a pilot-scale small decentralized sewage treatment: anaerobic filter + constructed wetland

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Resumen

En este estudio se midieron las emisiones de gases de efecto invernadero i.e. CH$_4$, CO$_2$ y N$_2$O, producidas en un sistema descentralizado de tratamiento de aguas residuales municipales (SDST). El sistema consistió de un filtro anaerobio (UAF) seguido de dos humedales construidos operando en paralelo plantados con Heliconia sp L. (HCW) y C. papyrus. (PCW). Las emisiones medidas en el UAF(1.8 - 8.9 g.m$^{-2}$.d$^{-1}$ CO$_2$; 8.3 y 45 g.m$^{-2}$.d$^{-1}$ CH$_4$) fueron mayores a las medidas en HCW (-5.1 y 5.5 gCO$_2$.m$^{-2}$.d$^{-1}$; 10 y 556 mgCH$_4$.m$^{-2}$.d$^{-1}$; -4 and 40 mgN$_2$O.m$^{-2}$.d$^{-1}$) y PCW(-0.85 to 6.5 gCO$_2$.m$^{-2}$.d$^{-1}$; 2.3 and 1590 mgCH$_4$.m$^{-2}$.d$^{-1}$; -7 y 12 mgN$_2$O.m$^{-2}$.d$^{-1}$). Las pruebas estadísticas indicaron que para el mismo fotoperiodo (día o noche) no hubo diferencias entre HCW y PCW. Adicionalmente, las variaciones de GEI pudieron ser explicados por la temperatura del agua, el fotoperíodo, la presencia de NH$_4^+$ y la concentración de OD. El incremento en temperatura del agua estimula la producción de GEI. Igualmente durante el fotoperiodo el secuestro de CO$_2$ y CH$_4$ fue favorecido. La presencia de NH$_4^+$ y cambios en el OD en HCW y PCW estimularon la producción de N$_2$O. En conclusión, los resultados indicaron que el sistema descentralizado fue una fuente neta de GEI emitiendo 0.7 kg CO$_2$eq. Kg COD$_{rem}$.

Palabras clave: Filtro anaerobio, gases efecto invernadero, humedales construidos, sistemas descentralizados de tratamiento de aguas residuales.

Abstract

Greenhouse gases such as CH$_4$, CO$_2$ and N$_2$O were measured in a Small-Decentralized Sewage Treatment (SDST). The system consisted of an up-flow anaerobic filter (UAF) and two constructed wetlands (CWs) operating in parallel. The constructed wetlands were planted with Heliconia sp L. (HCW) y C. papyrus. (PCW). The results showed that GHG average (daytime and nighttime) emissions from UAF (1.8 - 8.9 g.m$^{-2}$.d$^{-1}$ CO$_2$; 8.3 y 45 g.m$^{-2}$.d$^{-1}$ CH$_4$) were higher than measured in HCW (-5.1 y 5.5 gCO$_2$.m$^{-2}$.d$^{-1}$; 10 y 556 mgCH$_4$.m$^{-2}$.d$^{-1}$; -4 and 40 mgN$_2$O.m$^{-2}$.d$^{-1}$) and PCW(-0.85 to 6.5 gCO$_2$.m$^{-2}$.d$^{-1}$; 2.3 and 1590 mgCH$_4$.m$^{-2}$.d$^{-1}$; -7 y 12 mgN$_2$O.m$^{-2}$.d$^{-1}$). A statistical test showed that there were not significant differences between GHG flux (daytime-nighttime) measured in HCW and PCW (p<0.05). Further, the variations on GHG could be explained by water temperature, photoperiod, NH$_4^+$ and dissolved oxygen mainly. High temperature stimulates GHG production. Photoperiod in CWs increased CO$_2$ and CH$_4$ sequestration. Further, the presence of dissolved oxygen and NH$_4^+$ influenced N$_2$O production. Overall, in this study was determined that SDST act like a net source of GHG emitting 0.7 kg CO$_2$eq. Kg COD$_{rem}$.

Keywords: Anaerobic filter, constructed wetlands, greenhouse gases, small and decentralized wastewater treatment.
1. Introduction

The growing awareness of the impact of greenhouse gases such as CO$_2$, CH$_4$ and N$_2$O from human activities on climate change triggers the need to identify and quantify the main sources of these gases. According to Forster et al. (2007), a wide range of direct and indirect measurements confirm that the atmospheric mixing ratios of dioxide carbon (CO$_2$), methane (CH$_4$), and nitrous oxide (N$_2$O) have increased globally over the last 250 years by 36, 250, and 18%, respectively due to anthropogenic activities such as production and use of fossil fuels, industrial and agricultural activities, and waste management among others. Thus, compilation of data covering these sectors is the basis for collective action on the reduction of anthropogenic GHG emissions (UNFCCC, 2007).

Small-decentralized sewage treatment systems (SDST), such as up-flow anaerobic filter (UAF) + constructed wetlands (CWs), have been suggested as efficient low-cost and low-tech options for sewage treatment mainly in developing countries (Parkinson & Tayler, 2003; Vymazal, 2005; Massoud et al., 2009). SDST use little or no electrical energy, are more appropriate than energy-intensive processes, such as activated sludge, and they are cheaper to construct, operate and maintain. However, SDST may generate secondary negative environmental impacts because they might generate greenhouse gases such as carbon dioxide (CO$_2$), methane (CH$_4$) and nitrous oxide (N$_2$O) related to the intrinsic metabolic processes that occur during wastewater treatment (Inamori et al., 2007; Søvik & Klove, 2007). Hence, this study is aimed at: (1) measuring the emissions of CO$_2$ and CH$_4$, from SDST operating under tropical condition (2) to study the influences of environmental factors that regulate the emissions i.e. temperature. A special emphasis was given to estimate the differences between emissions during daytime (higher solar radiation) and night-time (lower solar radiation) conditions, and finally, this research was also aimed at contributing to reduce the knowledge gap on GHG emissions field data from SDST.

2. Methodology

2.1 Site description and experimental set up

This study was carried out in the experimental research station for wastewater treatment of Ginebra, a small town of 10,000 inhabitants located in Southwest Colombia ($3^\circ43'25.98\ N$, $76^\circ15'59.45\ W$). The historical average ambient temperature of this town is 26 $^\circ$C and its altitude is 1,040 m above sea level.

The system studied was a small-decentralized sewage treatment system (SDST) treating sewage wastewater. This system consisted of an up flow anaerobic filter (UAF) connected to two horizontals subsurface flow constructed wetlands (CWs) operating in parallel (Fig. 1). The constructed wetlands were planted with *Heliconia* sp. L. (HCW) y *C. papyrus*. (PCW). The system was constructed according to the characteristics shown in Table 1.
2.2 Wastewater sampling

The influent and effluent wastewater quality in both UAF and CWs was determined through 24-hour sampling campaigns carried out weekly. The day was divided in periods of eight hours. During each period a composite sample was collected by taking every hour a fixed volume of sample and add these together for analysis. Additional wastewater grab samples were taken in the central point of CWs, at the spot where GHG fluxes were measured, to determine the correlation between GHG fluxes and wastewater characteristics.

Chemical oxygen demand (COD), total suspended solids (TSS), alkalinity, total Kjeldahl nitrogen (TKN), ammonium nitrogen (N-NH$_4^+$), nitrate nitrogen (N-NO$_3^-$) were measured according to Standard Methods (APHA, 2005). Conductivity, pH, dissolved oxygen (DO), temperature and oxidation-reduction potential were measured with electrodes.

2.3 Greenhouse gas measurement

Greenhouse gas emissions (CH$_4$, CO$_2$ and N$_2$O) were measured in situ weekly during 6 months by using the technique of closed static chambers (Silva et al., 2015). GHG emissions from UAF were measured using a cylindrical acrylic transparent chamber with a diameter of 0.30 m height of 0.80 m and a volume around 21.4 l. On the other hand, to measure GHG emissions in CW was used a large chamber of 0.4 diameter, 0.9 m height, and 113 l volume. These dimensions permit contain whole plant body. In the constructed wetlands the chamber was fixed on a cylindrical base (D=0.4m), which was inserted to 10 cm depth and sealed by a water-filled ring on the slag surface. The chambers were installed only at the times of measurement.

The gas samples were measured at two different times of the day: between 12 am and 2 pm (day-time) and 10 pm and 12 pm (night-time). In UAF GHG samples were taken during 12 minutes at 4-minute intervals (0,4,8,12) whereas in CW the samples were
taken during 45 minutes at 15-minute intervals (0,15,30,45). The gas samples were taken out with syringes, which were withdrawn directly through a needle into a pre-evacuated vial.

These gas samples were subsequently analyzed. CO₂ was measured by an infrared spectrophotometer Qubit S151 CO₂ analyser (Loligo Systems, Denmark) using 75 ml min⁻¹ air as the mobile phase with a temperature of the injector set equal to the ambient temperature. CH₄ and N₂O were analyzed by gas chromatography (Shimadzu Co., Japan) equipped with a flame ionic detector (FID) and electron capture detector (ECD).

The fluxes were calculated using equation 1 from linear and no linear changes in the gas concentration in the chamber headspace (Silva et al., 2015).

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F = \frac{dC}{dt}_{t=0} \times \frac{V_c}{A} \times \frac{1440}{d}
\]

\(F\) = the flux of \(CH_4, CO_2, N_2O\) (gm⁻²d⁻¹); \(dC/ dt_{t=0}\) = slope of the gas concentration curve (gm⁻³min⁻¹); \(V_c\) = volume of the chamber (m³); \(A\) = the cross sectional area of the chamber (m²).

2.4 Data analysis

All statistical analyses Statistical were performed using SPSS® software (v. 17.0 for Windows). The Kolmogorov-Smirnov test was used to check normality of data. Further, an ANOVA analysis and Wilconson test (\(\alpha = 0.05\)) were used to compare the differences between daytime and night-time fluxes.

3. Results and discussion

3.1 Wastewater characteristics

Average COD and TKN concentrations measured in the influent were 333.1±110 mg COD.l⁻¹ and 40.2±4.28 mg TKN.l⁻¹. The removal efficiencies for COD and TKN in of SDST (UAF+CW) were 74 and 31.3 % respectively (Fig. 2). According to the statistical analysis there were no significant differences between HCW and PCW related to COD removal, TKN and NH₄⁺-N (p<0.05). As shown, COD removal was lower in UAF than obtained in HCW or PCW. On the other hand, TKN coming from UAF was removed by 31.3±10.1 and 26.2± 8.3 % for HCW and PCW respectively. In addition, NH₄⁺-N was removed in a 20.8±8.4 and 27.1±5.1 % for HCW and PCW respectively (Fig. 2). In UAF probably formed NH₄⁺-N was due to organic nitrogen hydrolysis in the effluent.

3.2 Greenhouse gas emissions from anaerobic filter

Figure 3 shows CH₄ and CO₂ fluxes measured in UAF during the monitoring campaign. As shown, UAF acted like a permanent source of CH₄ and CO₂. CO₂ fluxes during daytime ranged between 1.8 and 8.9 g.m⁻².d⁻¹ (median=5.3; SD=2.3; n=20) while at night-time they ranged from 1.8 and 4.1 g.m⁻².d⁻¹ (median=3.2; SD=0.8; n=20). According to the statistical test there were not significant differences between CO₂ produced in UAF during daytime and night-time (p<0.05). On the other hand, CH₄ fluxes for the daytime period ranged between 13 and 45 g.m⁻².d⁻¹ (median= 25.7; SD = 12.9; n= 20) while at night-time were ranging between 8.3 and 19.8 g.m⁻².d⁻¹ (median= 13.3; SD= 4.1; n=20). Comparison of CH₄ released fluxes in UAF for the periods day-time and night-time through the statistical test, showed significant differences in the emissions of this gas for both periods (p=0.026). Regarding to nitrous oxide the emissions in UAF were not detectable under experimental conditions.
The average emissions from UAF obtained in this study were lower than those reported in the literature for anaerobic lagoons operated under the Mediterranean climatic conditions (Toprak, 1995; Picot et al., 2003), tropical conditions (Silva et al., 2011) and operating at high organic loads (DeSutter & Ham, 2005; Yacob et al., 2005; Hasanudin et al., 2006; Konaté et al., 2013).

According to the amount of CH₄ produced and the COD removed was calculated that in UAF were produced 0.09 m³CH₄.kg⁻¹.COD removed⁻¹. This value was higher than the value of 0.06 m³CH₄.kg COD⁻¹ reported in an UAF treating low strength domestic wastewater and operating under similar conditions of OLR and temperature (Kobayashi et al., 1983), but lower than those observed in an UAF treating synthetic domestic sewage (0.15 m³CH₄.kg COD⁻¹) operating under psychrophilic conditions (15-17 °C)(Martin et al., 2010).

Results of statistical test indicated that the organic load rate (OLR) and water temperature influenced CH₄ fluxes (R²=0.79) while changes in CO₂ emissions were attributed to water temperature (R²=0.49). The positive correlation found among water temperature and GHG fluxes has been also observed in low strength wastewater anaerobic treatment (Langenhoff & Stuckey, 2000; Lettinga et al., 2001). An increase of temperature favours the anaerobic process by increasing the anaerobic bacteria activity and therefore CH₄ and CO₂ emissions are increased. In anaerobic treatment systems operating under high temperatures i.e. tropical conditions is expected a higher GHG production than systems under low temperature i.e. psychrophilic. However, the temperature not is the only operational variable that control GHG production. This can be observed in the fact that the emissions obtained from our study (Tw=27 C) were lower than reported in anaerobic reactor operating under psychrophilic conditions (Martin et al., 2010). This suggests that another operational factor such as the organic load rate also influence GHG production in anaerobic treatment systems. The low OLR (0.7 kg COD.m⁻³.d⁻¹) applied to UAF limited the concentration of active bacterial biomass in the reactor that influencing the low COD removal observed and decreasing in the CH₄ production (Chiang & Dague, 1992).

3.3 Greenhouse gas fluxes from HCW and PCW constructed wetlands

CO₂ Emissions

The fluxes of CO₂ from CWs measured during day-time and nigh-time were significantly different (p=0.041). Carbon dioxide fluxes in HCW (Fig. 4) during day-time ranged between -5.1 and 0.3 gCO₂.m⁻².d⁻¹ (median= -1.5; SD=1.6;n=20), while at nigh-time were measured values between 1.7 y 5.5 gCO₂.m⁻².d⁻¹.
In the Figure 4 are shown the methane flux from CW measured during daytime and night-time periods. In general, the emissions of CH4 in HCW were ranging during daytime between – 248 and – 84, whereas during night-time they were ranging from 49 to 716 µmol m⁻² s⁻¹. These differences between daytime and night-time CH4 emissions suggest that during the day the CWs systems behave as CH4 sinks while at night they produced this gas.

According to the statistical analysis the flux of CO2 from CWs was correlated to the water temperature (50.2%), environment temperature (27.2%) and water pH (10.3%). Thus, high water and environment temperatures regulated by tropical conditions increased CO2 emissions from CWs. The pH contributes to capture CO2 and to reduce the emissions of this gas in the CWs. Under alkaline conditions CO2 can be converted to bicarbonate alkalinity and probably this could favour less CO2 emissions. On the other hand, decreasing pH (6.8-7.2) lead to release more CO2 into the atmosphere.

**CH4 emissions**

In the Figure 4 are shown the methane flux from CW measured during daytime and night-time periods. In general, the emissions of CH4 in HCW were ranging during daytime between – 248 and – 84, whereas during night-time they were ranging from 49 to 716 µmol m⁻² s⁻¹. These differences between daytime and night-time CH4 emissions suggest that during the day the CWs systems behave as CH4 sinks while at night they produced this gas.
1240 mg CH$_4$.m$^{-2}$.d$^{-1}$ (median=375; SD=428.9; n=12). These emissions were higher than those measured for the night-time period which were ranging between 10 and 556 mgCH$_4$.m$^{-2}$.d$^{-1}$ (median=95; SD=222; n=12). In PCW the fluxes during the day-time varying between 2.3 and 1590 mgCH$_4$.m$^{-2}$.d$^{-1}$ (median=430; SD=448; n=12) while during night-time ranged from 80 to 640 mgCH$_4$.m$^{-2}$.d$^{-1}$ (median= 289.5; SD=162.7; n=12). On the other hand, the statistical test showed that there were no significant differences between the fluxes measured in both constructed wetlands (p=0.132). Therefore, CH$_4$ emissions for both wetlands considered at the current study were similar.

Methane emissions observed in this study were comparable to those observed in CW operating under subtropical climatic conditions treating domestic wastewaters (Johansson et al., 2004; Picek et al., 2007). Maximum flux values found were compatible with those found in studies with CW treating agricultural wastewater (Tanner et al., 1997; Vander Zaag et al., 2010). In addition, negative CH$_4$ flux values found in this study, coincided with those observed in other studies (Johansson et al., 2004; Teiter & Mander, 2005; Sovik & Klove, 2007; Ström et al., 2007). The flux of methane is the net difference among production and oxidation of this gas in the CW. A positive flux value of CH$_4$ indicates that there is generation of this gas, while a negative value indicates that there was consumption. Thus, CH$_4$ negative fluxes obtained in the CW under study, indicate that probably this gas was consumed which may be attributed to oxidation of methanotrophs that favours the oxidation of CH$_4$ (Inamori et al., 2007; Wang et al., 2013).

The correlation between environmental parameters and methane fluxes indicate that production of this gas in both CWs was mainly influenced by the water temperature (67.8%) and in a lesser proportion by the organic load applied (8.9%) and pH (7.4%). The high temperatures under tropical conditions increase the microbial activity and GHG were increased. The influences of temperature on GHG emissions have been also observed in different CW from Europe. The CH$_4$ emissions were higher during high temperature seasons (summer) that in low temperatures (winter)(Tanner et al., 1997; Johansson et al., 2004; Sovik et al., 2006; Picek et al., 2007; Vander Zaag et al., 2010). As reported Johansson et al. (2004) 33-43% of CH$_4$ flux variations were attributed to water temperature and sediments. Likewise, in a HSSF-CW treating municipal wastewater in Estonia, sediment temperature was the variable that showed a correlation positive related to CH$_4$ emissions (Teiter & Mander, 2005). By contrast, the results obtained on a CW treating mining runoff suggest that soil and water temperatures poorly explained the emission of GHG (Liikanen et al., 2006). In addition, the CH$_4$ fluxes were also positively correlated to the OLR. A higher load of organic matter (BOD, COD, TOC) contributes to provide larger substrate decomposition and to increase of more reducing zones in CW, favouring production of CH$_4$ (Gui et al., 2007; Inamori et al., 2007; Picek et al., 2007; Uggetti et al., 2012). Therefore the OLR influence methane production in CWs.

$\text{N}_2\text{O}$ emissions

In general $\text{N}_2\text{O}$ flux values indicated that constructed wetlands become an emitting source of this gas (Fig. 5). In HCW during day-time $\text{N}_2\text{O}$ flux ranged between -16 and 32 mgN$_2$O.m$^{-2}$.d$^{-1}$ (median= 9.1; SD=11; n=20), while for night-time the flux remained between -4 and 40 mgN$_2$O.m$^{-2}$.d$^{-1}$ (median=3.8; SD=12; n=20). On the other hand, in PCW for the daytime period the N$_2$O fluxes were ranging between -7 and 9 mgN$_2$O.m$^{-2}$.d$^{-1}$ (median=3; SD=4;n=20) whereas that at the night-time remained between 0 and 12 mgN$_2$O.m$^{-2}$.d$^{-1}$ (median=3;SD=3.8;n=20). It is important to clarify that negative nitrous oxide in this study was detected only once during the monitoring campaign. According to the statistical test there was no difference between the N$_2$O fluxes measured for daytime and night-time in both constructed wetlands. In addition, using the removed mass from TKN as N removal indicator it was calculated that those of ratio N2O-N/TKN for H-CW and C-CW were 0.3% y 0.1% respectively.
The N₂O fluxes from Ginebra CWs were in the range reported for FWS-CW in Sweden (Johansson et al., 2003; Ström et al., 2007), HSSF in Norway (Sovik & Klove, 2005), Czech Republic (Picek et al., 2007) and Finland (Liikanen et al., 2006; Sovik et al., 2006). However, in CW treating dairy wastewater (Tanner et al., 1997; Vander Zaag et al., 2010) and municipal wastewaters (Inamori et al., 2007) lower values of N₂O were obtained compared with CWs studied at the current research. On the other hand, N₂O flux values reported by Uggeti et al. (2012) for a CW treating waste activated sludge were 20 times higher than the estimated in this study.

N₂O in constructed wetland is mainly produced by nitrification, denitrification, and denitrifier denitrification (Wrage et al., 2001): (i) Nitrifiers i.e. ammonia-oxidizing bacteria (AOB) produce N₂O mainly by the incomplete oxidation of hydroxylamine and by nitrifier denitrification. In nitrifier denitrification, the oxidation of NH₃ to NO₂⁻ is followed by the reduction of NO₂⁻ to N₂O and N₂. In the case of nitrification the N₂O is formed during incomplete NH₄⁺-N oxidation to NO₃—N by low DO concentration (Zeng et al., 2003). (ii) Denitrifiers produce N₂O as an intermediate possible end product of the reduction of NO₃⁻-N to N₂. Nitrous oxide is formed by incomplete denitrification related to the availability of nitrate (Sovik et al., 2006), increase of oxygen in water (Von Schulthess et al., 1994), or low COD/N ratio (3.5) (Hanaki et al., 1992).

According to statistical test NH₄⁺ could explain 23.2 % on the variation of the N₂O emitted from CWs. Removal of NH₄⁺ in both HCW and PCW suggests that nitrification and subsequent denitrification were carried out in these systems. During nitrification AOB bacteria, which are the dominant microorganisms of the rhizosphere (Huang et al., 2013) may produce NO and N₂O either as a side-product in the catabolic pathway (oxidizing ammonia to nitrite), or, alternatively, by denitrification of nitrite with ammonia, hydrogen or pyruvate as electron donor (Colliver & Stephenson, 2000; Wrage et al., 2001; Law et al., 2012). In addition, the NO₃⁻ formed during nitrification may be reduced to NO₂ by incomplete denitrification due to the presence of some amount of oxygen in the wetland. In this study both CW’s was negatively correlated with dissolved oxygen explaining 22% of N₂O variation. As reported in conventional wastewater treatment systems the N₂O formation via denitrification increases when DO levels are increased (Von Schulthess et al., 1994). For instance, it has been reported that a concentration of DO around 0.09 mg.l⁻¹ decreased the denitrification rate by 35% and under DO concentrations around of 5.9 mg.l⁻¹ practically the denitrification fell down to zero (Oh & Silverstein, 1999). Summarizing, the formation of N₂O in HCW y PCW probably was influenced by both the nitrification and denitrification process. The temperature could explain 34.3 % on the variation of the N₂O fluxes.

In this study the CWs were operated under tropical conditions characterized by high temperatures, which probably favored more N₂O production. The influence of the temperature on N₂O fluxes from CWs was observed in different CW operating in Europe (Johansson et al. 2003; Teiter & Mander 2005; Liikanen et al. 2006; and Sovik & Klove 2007). In this studies was reported that low temperatures slow down the nitrification process since the activity of ammonia oxidizing bacteria decrease and also the denitrification is limited.

3.4 Overall GHG emissions from small-decentralized system (UFA + CW)

The greenhouse gas emissions in terms of grams of CO₂eq m⁻² d⁻¹ are reported in Table 3. According
to the CO$_2$e calculated, methane is the GHG that offers more contribution to GWP in the small-decentralized wastewater treatment system. In general, on the basis of CO$_2$e, CH$_4$ represents 99% of total emissions of the whole treatment. CH$_4$ to CO$_2$ ratio for the whole treatment system was 91 while the ratio of CH$_4$ to N$_2$O was 178.9. Moreover, calculation of ratios CH$_4$/ N$_2$O for H-CW and C-CW reported average values of 8.3 and 3.1 respectively. This suggests that upon combining anaerobic technologies and systems such as the CW (Hasanudin et al., 2006) is the major ecological footprint is attributed to the GHG generated in the anaerobic i.e. CH$_4$.

Moreover, calculation of ratios CH$_4$/ N$_2$O for H-CW and C-CW reported average values of 8.3 and 3.1 respectively. This suggests that upon combining anaerobic technologies and systems such as the CW (Hasanudin et al., 2006) is the major ecological footprint is attributed to the GHG generated in the anaerobic i.e. CH$_4$.

Comparing the CO$_2$e for two wetlands, it is concluded that there was no significant difference in their impact to GWP. Moreover, upon comparing carbon and nitrogen rates of transformation to CH$_4$ and N$_2$O in HCW y PCW, these were lower. The foregoing suggests that only a small amount of carbon and nitrogen removed is transformed to CH$_4$ minimizing the generation of this GHG in CWs studied. The 3% value of carbon transformed into CH$_4$ obtained in this study was lower than reported for different European wetlands (Søvik et al., 2006; Søvik & Klove, 2007). On the other hand, the ratios of N$_2$O-N emissions to TKN removal are within the range of that reported by different studies in CW (Johansson et al., 2003; Søvik et al., 2006; Søvik & Klove, 2007).

### 4. Conclusions

This study has provided information about GHG emissions from decentralized wastewater treatment system operated under tropical conditions. According to the results, SDST was a net source of CO$_2$, CH$_4$ and N$_2$O, having to UAF as the treatment unit that offers a higher contribution to GWP than constructed wetlands. Thus, reducing the environmental impact of UAF involve capture and recover of methane via energy production or flared to avoid its release into the atmosphere. On the other hand, the GWP determined for CWs suggest that this technology had lower environmental impact than anaerobic technology.

A significant difference between CO$_2$ fluxes measured in CW during day-time and night-time periods was observed in this study. This suggest that CO$_2$ emissiosn from CWs operating under tropical conditions are influenced by the photoperiod. Thus, during photo period CW are net sink and therefore these systems can act as regulators of atmospheric CO$_2$ reducing their environmental impact(GWP).

A similar pattern due to the photoperiod was observed in CW related to methane production. The oxygen translocated into the roots probably inhibited methane release into the atmosphere via methane oxidation by methanotrophs. Based on results, a next step would be to adress experimental setup to determine the influence on methane emissions due to methane oxidation process.

The results found adress the necessity to follow researching about the real impacts of wastewater treatment systems from perespective of their GWP contribution.

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### 6. References

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